

## AMENDMENTS TO THE SPECIFICATION

Please replace paragraph number [0032] with the following rewritten paragraph:

A first embodiment of a method according to the invention is described with reference to FIGS. 1 and 2. First, the mixing vessel 110 is charged with a quantity of a suitable polymer, wax and/or lipid, which is referred to in FIG. 2 as a "carrier material" (step 200). The mixing vessel 110 is closed and sealed. The controller 184 activates the supercritical fluid pump 114 to supply a quantity of supercritical fluid through the surge tank 140, through the metering valve 142, and into the mixing vessel 110 (step 202). The addition of the supercritical fluid by the supercritical fluid pump 114 increases the pressure P1 in the mixing vessel 110 to a predetermined pressure. The thermostat 180 and the supercritical fluid pump 114 cooperate to maintain the temperature and the pressure P1, respectively, in a generally constant desired operating range. Accordingly, the pressure P1 is generally in a range that is increased relative to atmospheric pressure, and is maintained in a predetermined range so the supercritical fluid remains in a supercritical state. Optionally The carrier material (i.e., the polymer, wax and/or lipid) can contact the supercritical fluid in the mixing vessel 110 in the absence of any solvents or, optionally, the controller 184 controls the co-solvent pump 112 to supply one ~~ore~~ or more co-solvents into the mixing vessel 110.

Please replace paragraph number [0035] with the following rewritten paragraph:

In the first embodiment of a method according to the invention, the contents of the mixing vessel 110 are expanded across a pressure drop through the nozzle 164 and into the expansion chamber 170. The supercritical fluid 172 flashes into a gas leaving composite particles 174 comprising the polymer, wax and/or lipid and the solute. The solvent

present during expansion is removed from the expansion chamber by the process of evaporation. The temperature of the expansion chamber is maintained above the boiling point of the solvent and monitored in order to facilitate the removal of the solvent from the expansion chamber. The pressure P2 in the expansion chamber 170 is preferably at or near atmospheric pressure. Optionally, the controller 184 can control the pressure P2 to be increased relative to atmospheric pressure by using the backpressure regulator 162. By manipulating the pressure differential, the size and configuration of the nozzle 164, and the rate at which the first fraction is allowed to flow from the mixing vessel 110 to the expansion chamber 170, the size and morphology of the resultant particles can be controlled. Generally, the larger the pressure differential, the smaller the resultant particles that are produced. Accordingly, the pressure P2 can be maintained at a pressure that is lower than atmospheric pressure in order to increasing the pressure differential.